Small angle X-ray scattering measurements probe water nanodroplet evolution under highly non-equilibrium conditions†

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Our in situ small angle X-ray scattering (SAXS) measurements yield an unprecedented and detailed view of rapidly evolving H$_2$O nanodroplets formed in supersonic nozzles. The SAXS experiments produce spectra in a few seconds that are comparable to small angle neutron scattering (SANS) spectra requiring several hours of integration time and the use of deuterated compounds. These measurements now make it possible to quantitatively determine the maximum nucleation and growth rates of small droplets formed under conditions that are far from equilibrium. Particle growth is directly followed from about 10 $\mu$s to 100 $\mu$s after particle formation with growth rates of $\sim$0.2 to 0.02 nm $\mu$s$^{-1}$. The peak H$_2$O nucleation rates lie between $10^{17}$ and $10^{18}$ cm$^{-3}$ s$^{-1}$.

Introduction

Supersonic nozzles are a convenient way to produce and study high number density aerosols comprised of droplets in the nanometer size range. With nozzle cooling rates on the order of 0.5 K $\mu$s$^{-1}$, the vapor reaches high supersaturations, and particle formation and growth occur far from equilibrium. Prior explorations of nanodroplet evolution in nozzles have been limited by the standard experimental techniques, including pressure measurements and light scattering, because these techniques do not provide detailed information regarding particle size distributions. Thus, data to spur the development of better theories for nucleation, particle growth, and coagulation under highly non-equilibrium conditions are generally not available. In this paper we describe the use of small angle X-ray scattering (SAXS) to directly determine the nucleation and growth rates of nanoparticles in supersonic nozzles similar to those used previously. Although these experiments focus on water nanodroplets, many of the issues we address are germane to the production of monodisperse nanoparticles by other aerosol routes.

In our earlier work we used small angle neutron scattering (SANS) to characterize the D$_2$O aerosols formed in supersonic nozzles. In contrast to long visible light (~500 nm), the wavelengths of neutrons (0.2–1 nm) and X-rays (~0.1 nm) are smaller than the droplets (average radius $r_i$ ~10 nm). Thus, SANS and SAXS spectra have structure that can be fit to determine the mean particle radius, $\langle r \rangle$, the width of the distribution $\sigma$ or its polydispersity $\xi = \sigma / \langle r \rangle$, and the number density $N$ of the aerosol. As we show here, the small (0.2 mm $\times$ 0.2 mm), highly monochromatic ($\Delta \lambda / \lambda = 10^{-4}$) X-ray beam with its high photon flux overcomes the time and resolution limitations inherent in our SANS studies and makes detailed studies of particle formation and evolution in supersonic flows entirely practical. Our work complements that of others who have used SAXS to examine the evolution of soot and metal oxide nanoparticles produced in flames.

Experimental

The apparatus used in this work has been described in detail in Tanimura et al. and is only summarized briefly here. A dilute mixture of water vapor (<6 mol%) in N$_2$ carrier gas, initially at stagnation pressure $p_0$ and stagnation temperature $T_0$, expands as it flows through a supersonic Laval nozzle. As the gas cools, the supersaturation increases rapidly and particles begin to form by homogeneous nucleation. Eventually, the particle formation rate is high enough that growth of the newly formed droplets rapidly depletes the vapor, and the latent heat released increases the temperature and pressure of the gas. Both effects quench nucleation, although depletion is far more important.

We characterize the condensation process by making extensive static pressure measurements along the axis of the nozzle for different combinations of $T_0$ and the mass flow rate of water entering the nozzle. We hold $p_0$ constant by reducing the flow rate of N$_2$ as the flow rate of water increases. For these dilute gas mixtures the total molar flow rate through the nozzle is approximately constant. A dry pressure trace (N$_2$ flow only) defines the effective area ratio $A / A^*$ of the nozzle. To determine the temperature, density, and velocity in the condensing flow, we integrate the diabatic flow equations using the stagnation conditions, the condensing flow pressure trace, and the effective area ratio as input. We also assume that $A / A^*$ is not affected by the condensation process.

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† The HTML version of this article has been enhanced with colour images.
of this assumption is discussed by Tanimura et al. Analysis of the pressure data yields the pressure and temperature corresponding to the peak nucleation rate and shows that, depending on the nozzle and flow conditions, the nucleation bursts last between 7 and 15 \mu s.

We investigated two Laval nozzles, H2 and C2, characterized by the effective expansion rates of \( d(A/A^*)/dx = 0.054\ \text{cm}^{-1} \) and \( d(A/A^*)/dx = 0.078\ \text{cm}^{-1} \), respectively. These nozzles have rectangular cross sections with a constant width equal to 1.2 cm, and the height at the throat is 0.5 cm. The top and bottom walls of the nozzle converge and diverge symmetrically. The straight converging section (~2 cm long, ~20° half angle) and the straight diverging section (~9.5 cm long, 0.89° or 1.5° half angle) are joined near the throat by a ~2.5 cm long cubic section. The cubic is chosen so that the expansion in the supersonic region is continuous through the second derivative. A photograph of a similar nozzle is given in Fig. 2 of Wyslouzil et al. For \( \text{H}_2 \text{O} \) condensation, \( p_0 \) was fixed at 30 kPa and \( T_0 \) was 298 K (nozzle H2) or 308 K (nozzle C2). A limited number of experiments were conducted with \( \text{D}_2\text{O} \) using nozzle C2 and here \( (p_0, T_0) = (60 \text{ kPa, 308 K}) \). The expansion rate of nozzle C2 is very close to that of nozzle C used by Kim et al., and the stagnation conditions are the same. We can, therefore, directly compare the current SAXS measurements to our earlier SANS results.

All SAXS measurements were made at the Advanced Photon Source at Argonne National Laboratory on the Besserec 12-ID beam line 11 using 12 keV X-rays (\( \Delta \lambda/\lambda = 10^{-4} \)) and a sample to detector distance (SDD) of 2.0 m. The X-ray windows were made by machining 1 mm \( \times \) 90 mm slits into the nozzle side walls and then covering these slits by gluing 25 \( \mu \)m thick ruby mica sheets (10 mm \( \times \) 100 mm) to the inside of the aluminium side walls with epoxy. The range of the momentum transfer vector \( q \), where \( q = (4\pi/\lambda)(\sin\theta/2) \) and \( \theta \) is the scattering angle, was calibrated by scattering from a sample of silver behenate. We used the APS data reduction program to correct for the dark background, the pixel efficiency and spatial inhomogeneities on the detector. To produce the radially averaged spectra, the pixels were binned logarithmically (four pixels per bin) to improve the statistics, especially at high \( q \).

### Results and discussion

In Fig. 1, we directly compare our current measurements with two \( \text{D}_2\text{O} \) scattering spectra measured by Kim et al. 4 using SANS, after the latter have been corrected for the increased scattering length densities of X-rays over neutrons, \( (\Delta \rho_{\text{D}_2\text{O,X-ray}}/\Delta \rho_{\text{D}_2\text{O,neutron}}) \). Because the absolute calibration procedures for SANS are more firmly established than those for SAXS, we can force agreement between the two measurements to place the SANS results on an absolute intensity scale. The dashed lines are the X-ray data plotted on the scale used during the preliminary data evaluation. Multiplying the original SANS data by 4.6 gives an excellent match between the SANS and SAXS data sets except in the low \( q \) region where the SANS data consistently lie above the SAXS data. 13 The difference at low \( q \) is a consequence of the effective higher polydispersity of the aerosol resulting from the 12 mm wide viewing volume in the SANS experiment versus the nearly point measurements in SAXS. We estimate the accuracy of our calibration procedure to be \( \pm 20\% \) based on a \( \sim 10\% \) uncertainty for the original NIST calibration and \( \sim 10\% \) uncertainty in reproducing the experiments and determining the correction factor.

Each of the \( \text{D}_2\text{O} \) spectra measured using SANS required ~2 h of integration time (1 h for the sample, 1 h for the empty nozzle) at each sample to detector position. Thus, the SANS spectrum in Fig. 1(a) required 4 h of integration rather than the ~10 s (5 s sample, 5 s empty nozzle) required for the SAXS measurements.
spectrum measured at a single sample to detector position. At high water flow rates the SAXS data cover ~5 orders of magnitude in intensity over the accessible range of $q$. The inflection in the spectra at intermediate $q$ corresponds to the Bessel function minimum, and in the high $q$ region the intensity decreases as $q^{-4}$—features characteristic of scattering from a polydisperse distribution of spheres in bulk contrast. As the flow rate of D$_2$O decreases, Fig. 1b, the inflection moves to larger $q$ and the intensity at low $q$ drops, consistent with the expected decrease in average particle size as the volume of condensible material entering the nozzle is reduced. For nanodroplets consisting of one component, SAXS is clearly preferable to SANS because it is significantly faster, does not require expensive deuterated materials, and covers a wider $q$-range for a single detector position. Furthermore, because the speed of light is so much higher than the droplet speed, the Doppler shift correction$^{14}$ made for neutron scattering is not needed here.

Estimates for the parameters of the aerosol size distribution are easily obtained by fitting the spectra to polydisperse distributions of spheres. Here we used a Schultz distribution$^{15}$ to determine the average particle radius $\langle r \rangle$, the width of the size distribution $\sigma$ and the scattered intensity as $q \rightarrow 0$, $I_0$. When the data are on an absolute intensity scale, the aerosol number density $N$ is derived from $I_0$ using$^{16}$

$$N = \frac{3}{4\pi} \left( \frac{(z+1)^5}{(z+6)(z+5)(z+4)(z+3)(z+2)} \right) \left( \frac{I_0}{\langle r \rangle^6 (A_p)^2} \right)$$

where $z = ((\sigma^2)/\langle r \rangle^2) - 1$. The error bars associated with the parameters were determined as follows. For each experimental condition we combined two 5 s sample and two 5 s local background measurements in different ways to yield 4 spectra. We then fit these spectra to determine values for $\langle r \rangle$, $\sigma$ and $N$. We averaged the values for the fit parameters, and the error bars represent one standard deviation from the mean.

In Fig. 2 we compare the values of $N$, $\langle r \rangle$ and $\sigma$ as a function of the D$_2$O mass flow rate derived from the SANS and SAXS experiments. The agreement between the two data sets, taken ~3 years apart, at different facilities and using two different detection methods is remarkable. The average particle sizes are almost identical, the values of $N$ are close, and the widths of the distributions measured using SANS are only 12–16% higher than those measured by SAXS. One reason for the latter is the wider viewing volume used in the SANS experiments, and another, as we will show below, is the continued slow growth of the droplets, even near the nozzle exit. Thus, even with identical values of $\langle r \rangle$, contributions to the SANS scattering pattern from smaller droplets entering and larger droplets leaving the 12 mm wide viewing volume will effectively broaden the size distribution.$^{17}$

A series of similar SAXS measurements was made for H$_2$O using two nozzles characterized by different expansion rates. Fig. 3 summarizes the variation in $\langle r \rangle$, $\sigma$ and $N$ at a fixed location in the nozzle with the mass flow rate of water. For both nozzles there is a systematic increase in $\langle r \rangle$ and $\sigma$ and, initially, a decrease in $N$ with $m$$_{H_2O}$. Furthermore, the droplets formed in the more rapidly expanding nozzle C2 are significantly smaller, the distribution width is narrower, and the number density is higher than the droplets formed in nozzle H2. These observations are consistent with the fact that faster expansion rates lead to both higher nucleation rates and somewhat shorter nucleation bursts.$^5$ With a fixed initial amount of condensible material, the droplets are necessarily smaller as the number of droplets increases. In nozzle C2, the increase in $N$ with mass flow rate at higher $m$$_{H_2O}$ is unexpected, and we are exploring this effect in more detail by modelling the nucleation and growth process in our nozzles.

As illustrated in Fig. 4(a), we also characterized H$_2$O droplets as a function of the distance downstream of the throat at a fixed water flow rate of 5 g min$^{-1}$. Because the size of the X-ray beam is only 0.04 mm$^2$, these are essentially point measurements, and as a consequence we can easily resolve particle growth spatially, or equivalently, temporally. Note that in our nozzles, the velocity of the gas is ~400 m s$^{-1}$, and 1 mm corresponds to a flow time of ~2.5 μs. The pressure trace measurements corresponding to this liquid flow rate show that the peak nucleation rate occurs about ~1.5 cm downstream of the throat. Our first observation position for particles is ~2 cm downstream of the throat and, thus, we first

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**Fig. 2** The Schultz size distribution parameters, (a) average radius $\langle r \rangle$, distribution width $\sigma$, and (b) number density $N$, for D$_2$O aerosols measured ~5.6 cm downstream of the throat in nearly identical nozzles using SAXS (open symbols) and SANS (filled symbols). The error bars are only shown for points where they are larger than the symbol size. The SANS measurements$^4$ were made using the NG7-SANS at the NIST Center for Neutron Research.
observe droplets $\sim 10 \mu$s after they have formed. The mean radius $\langle r \rangle$ of the aerosol then increases from $\sim 3.5$ to $8 \text{ nm}$ over a distance of about $3.5 \text{ cm}$, or in $\sim 90 \mu$s.

From the pressure trace measurements we also determine the local gas velocity, which allows us to convert position in the nozzle into flow time downstream of the throat. Calculating the mean droplet growth rate is then straightforward and Fig. 4(b) summarizes our results. The highest average growth rate, $\langle \text{d}r/\text{d}t \rangle$, of the droplets we observe here is $0.17 \text{ nm m/s}$/C0. The growth rate drops to $0.02 \text{ nm m/s}$/C0 within $40 \mu$s primarily due to vapor depletion.

In contrast to the $200\%$ increase in $\langle r \rangle$, the width of the distribution $\sigma$ only increases about $30\%$, from $\sim 1.3$ to $1.7 \text{ nm}$, between the first and last observation points. The particle size distribution is, therefore, found to dramatically “narrow” as the aerosol evolves, $i.e.$, $\zeta$ decreases from 0.37 to 0.21. The width of the aerosol size distribution is a direct consequence of the length of the nucleation burst and the particle growth rate, since particles formed at the beginning of the nucleation burst grow significantly larger than the last particles formed. However the relative “birth advantage” is lost as the growth time increases and the average particle size gets large compared to the distribution width. For aerosols with a narrow size distribution, both coagulation and Ostwald ripening act to increase $\sigma$. Given enough time, coagulation leads to self-preserving size distributions with effective widths larger than those observed here. Simple coagulation estimates suggest that $N$ should only decrease by $5\text{–}10\%$ as the aerosol moves through the nozzle. For monodisperse droplets coagulating in the free molecular regime, Vermury et al. estimated the time required to reach the self preserving size distribution was 14 times that required to halve the initial number density. Thus, we expect the particles to remain relatively monodisperse as they exit the nozzle.

![Fig. 3](image1.png)

(a) The average particle size and the width of the size distribution both increase with the initial mass flow rate of condensible while (b) the number density of droplets initially decreases. The measurement location is $\sim 5.6 \text{ cm}$ downstream of the throat. The behavior of $N$ at higher flow rate may depend on nozzle shape and operating conditions. Nozzle C2 has a higher expansion rate, leading to higher nucleation rates, higher aerosol number densities and smaller droplet sizes than in nozzle H2.

![Fig. 4](image2.png)

In this experiment the water flow rate was 5 g min$^{-1}$, and $T_0$ and $p_0$ were 298 K and 30 kPa, respectively. (a) The average size $\langle r \rangle$ of H$_2$O droplets increases rapidly as a function of the distance downstream of the throat while the width $\sigma$ of the distribution remains relatively constant. The short dashed lines are the temperatures corresponding to an isentropic expansion of the gas mixture (lower curve) and the temperature of the condensing flow (upper curve). These temperatures are derived from static pressure measurements as described in the text. The period of rapid particle growth corresponds closely to the rapid increase in temperature of the gas stream. (b) The mean droplet growth rates were calculated from adjacent observation points as the difference in the mean droplet size divided by the difference in time. The latter uses the local gas velocity that is derived from the static pressure measurements. The growth rates are plotted at the time that corresponds to the location midway between adjacent measurements.
nucleation rates determined for the H$_2$O experiments. In comparable nozzle. D$_2$O condensation in a slightly slower nozzle. For nozzle C2, consistent with the result first observed by Khan gently test non-isothermal droplet growth laws under highly rapidly. These growth measurements will allow us to strin-
spatially resolved along the nozzle axis, and the mean radius temperature corresponding to the peak nucleation rate, and
factors of 2 as the temperature decreases, consistent with the rates are higher than in nozzle H2 and decrease by about a
time measurements as described in Kim et al.$^4$ Fig. 5 summarizes the nucleation rates determined for the H$_2$O experiments. In nozzle H2 the peak nucleation rate is essentially constant, consistent with the result first observed by Khan et al.$^{20}$ for D$_2$O condensation in a slightly slower nozzle. For nozzle C2, the rates are higher than in nozzle H2 and decrease by about a factor of 2 as the temperature decreases, consistent with the observations of Kim et al.$^4$ for D$_2$O nucleation rates in a comparable nozzle.

Summary and conclusions
We have shown that SAXS is a fine way to determine the size distributions of rapidly evolving aerosols formed in supersonic nozzles. For pure or well-mixed nanodroplets, SAXS experiments yield spectra in a few seconds that are comparable to SANS spectra requiring several hours of integration time and the use of deuterated compounds. The narrow X-ray beam also permits the size distributions of H$_2$O droplets to be spatially resolved along the nozzle axis, and the mean radius can be reliably determined even when the droplets are growing rapidly. These growth measurements will allow us to stringently test non-isothermal droplet growth laws under highly non-equilibrium conditions. We can also determine nucleation rates for a wide range of hydrogen-rich compounds, such as the n-alcohols and n-alkanes typically used in vapor–liquid nucleation research. The high rates characteristic of nozzles, $J \sim 10^{14}$ cm$^{-3}$ s$^{-1}$, provide a stringent test of extant nucleation rate theories. Accurate nucleation and growth rate theories are needed to assist the development of challenging technical applications such as the production of metal nanoparticles in supersonic nozzles where hostile operating conditions make measurements extremely difficult.

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References
12 Making the height of the mica sheet greater than the distance separating the nozzle blocks ensures that the inner surface of the nozzle is smooth in the supersonic region and, thus, avoids introducing weak shocks into the flow. The strength of the thin mica sheets limits the height of the side wall slit to 1 mm.
13 The multiplicative factor of 4.6 was necessary because the scale used in the initial SAXS data evaluation was not based on an absolute calibration standard. The scale factor for the SANS data is based on an absolute calibration procedure.
17 Aerosol polydispersity may also be affected by the presence of boundary layers next to the nozzle walls. Model calculations by Schnerr et al.$^{16}$ found that within the boundary layer nucleation
occurred further downstream as the wall was approached. The average particle size, however, rapidly approached that of the aerosol in the main stream. Based on the measurements of Tanimura et al., we estimate that at most 5% of the aerosol is formed more than 1 cm downstream of the particle formation event in the main stream. The observed polydispersity, therefore, is a result of the inherent polydispersity of the aerosol, modified slightly by particle formation in the boundary layer, and of the resolution functions of the instruments including the aperture size, the wavelength distribution, and the finite pixel size. The instrument factors associated with X-ray scattering are all much smaller than those of our earlier neutron scattering studies.